

## Chapter Five

### Dynamics of Fluid Flow

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#### **5.1 / Introduction :**

This chapter includes the study of forces causing fluid flow. Thus dynamics of fluid flow is the study of fluid motion with the forces causing flow.

#### **5.2 / Equation of motion :**

According to Newton's second law of motion , the net force  $F_x$  acting on a fluid element in the direction of  $x$  is equal to mass (  $m$  ) of the fluid element multiplied by the acceleration (  $a$  ) in the  $x$  – direction. Thus mathematically :

$$F_x = m a_x \quad ( 5 . 1 )$$

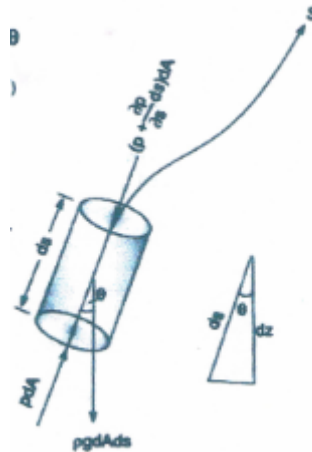
#### **5.3 / Euler's equation of motion :**

This equation of motion in which the forces due to gravity and pressure are taken into consideration. This is derived by considering the motion of the fluid element along a stream – lines as :

Consider a stream – line in which flow is taking place in  $S$  – direction as shown in Fig.( 5.1) . Consider a cylindrical element of cross – section  $dA$  and :

1. Pressure force (  $p dA$  ) in the direction of flow .
2. Pressure force (  $p + \frac{\partial p}{\partial s} ds$  )  $dA$  opposite to the direction of flow .
3. Weight of element (  $W = \gamma V = \rho g V = \rho g dA dS$  ) .  $a_s = \frac{dv}{dt} = \frac{v \partial v}{\partial s}$

[ ( Note : ( where  $v$  is a function of  $s$  &  $t$  , so , and (  $\cos \Theta = \frac{dz}{ds}$  ) ].



**Fig.( 5.1)**

$$\mathbf{F} = \mathbf{m} \mathbf{a}$$

$$\sum \mathbf{F} = \mathbf{m} \mathbf{a}$$

$$p dA - \left( p + \frac{\partial p}{\partial s} ds \right) dA - \rho g dA dS \cos \Theta = \rho dA ds \cdot \frac{v \partial v}{\partial s}$$

$$\frac{dp}{\rho} + g dz + v dv = 0 \quad (5.2)$$

**Equation (5.2)** is known as Euler's equation of motion .

In which ,  $p$  – pressure ,  $\rho$  – mass density ,  $g$  – gravity ,  $z$  – head ,  $v$  – velocity .

**5.4 / Bernoulli's equation from Euler's equation :**

Bernoulli's equation is obtained by integrating the Euler's equation of motion (5.2) :

$$\int \frac{dp}{\rho} + \int g dz + \int v dv = \text{constant}$$

If flow is compressible ,  $\rho$  is constant and :

$$\frac{p}{\rho} + g z + \frac{v^2}{2} = \text{constant}$$

$$\frac{p}{\rho g} + z + \frac{v^2}{2g} = \text{constant} \quad (5.3)$$

Equation ( 5.3 ) is a Bernoulli's equation , in which ,

$\frac{p}{\rho g}$  - pressure energy per unit weight of fluid ( pressure head )

$\frac{v^2}{2g}$  - kinetic energy per unit weight of fluid ( kinetic head ).

$Z$  - potential energy per unit weight of fluid ( potential head ).

**Assumptions :**

The following are the assumptions made in the derivation of Bernoulli's equation :

1 – The fluid is ideal ( viscosity is zero ).

2 – The flow is steady . (  $\frac{\partial v}{\partial t} = 0$  )

3 - The flow is incompressible. (  $\rho = \text{constant}$  ) .

4 – The flow is irrotational .

#### 5.5 / Bernoulli's equation for real fluid :

In real fluid , there are some losses , these losses have to be taken into consideration . Thus the Bernoulli's equation for real fluids between points 1 and 2 is given as :

$$\frac{p_1}{\rho g} + \frac{v_1^2}{2g} + z_1 = \frac{p_2}{\rho g} + \frac{v_2^2}{2g} + z_2 + H_L \quad (5.4)$$

In which  $h_l$  is loss of energy ( head loss ) between points 1 & 2 .

#### 5.6 / Instruments for measure the rate of flow :

1 – Venture meter .

2 – Orifice meter

3 – Pitot - tube .

#### 1 – Venture meter :

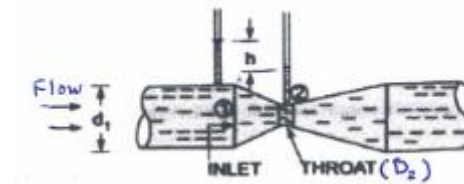


Fig.(5.2)

A venture meter is a device used for measuring the rate of a flow of a fluid flowing through a pipe. It consists of three parts :

( 1 ) short converging part , ( 2 ) Throat , ( 3 ) Diverging part .

It is based on the principle of Bernoulli's equation.

Applying Bernoulli equation at section 1 & section 2 ( throat ) , we get :

$$\frac{p_1}{\rho g} + \frac{v_1^2}{2g} + Z_1 = \frac{p_2}{\rho g} + \frac{v_2^2}{2g} + Z_2$$

As pipe is horizontal , hence  $Z_1 = Z_2$

$$\frac{p_1}{\rho g} + \frac{v_1^2}{2g} = \frac{p_2}{\rho g} + \frac{v_2^2}{2g}, \quad \frac{p_1 - p_2}{\rho g} = \frac{v_2^2}{2g} - \frac{v_1^2}{2g}$$

$\frac{P_1 - P_2}{\rho g}$  is the difference of pressure heads at section 1 & section 2

And it is equal to( h ) :

$$h = \frac{V_2^2}{2g} - \frac{V_1^2}{2g} \quad (5.5)$$

Now , applying continuity equation at section 1 & 2 :

$$A_1 V_1 = A_2 V_2 \quad , \quad V_1 = \frac{A_2 V_2}{A_1}$$

Substituting the of  $V_1$  in the equation (5.5) ,

$$h = \frac{V_2^2}{2g} \left[ \frac{A_1^2 - A_2^2}{A_1^2} \right]$$

$$V_2^2 = 2g h \frac{A_1^2}{A_1^2 - A_2^2}$$

$$V_2 = \frac{A_1}{\sqrt{A_1^2 - A_2^2}} \sqrt{2gh}$$

But ,  $Q = A_2 V_2$

$$Q = \frac{A_2 A_1}{\sqrt{A_1^2 - A_2^2}} \sqrt{2gh} \quad (5.6)$$

Where ,

X - reading of differential manometer .

$S_h$  – Sp.gravity of the liquid manometer .

$S_o$  – Sp.gravity of the liquid flowing through pipe .

## 2. Orifice meter :

It is a device used for measuring the rate of flow of a fluid through a pipe. It also works on the same principle as that of venturimeter. It consists of a flat circular plate which has a circular sharp edged hole called orifice , which is concentric with the pipe . The orifice diameter is kept generally 0.5 times the diameter of the pipe ( or 0.4 to 0.8 times the pipe diameter ) .

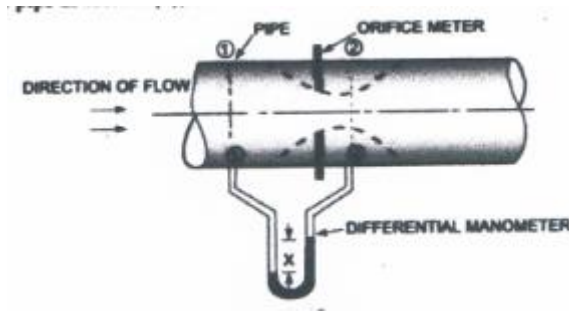


Fig.(5.3)

Applying Bernoulli equation between section 1 & section 2 , we get :

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2$$

As the pipe is horizontal ,  $Z_1 = Z_2$

$$\frac{P_1}{\rho g} - \frac{P_2}{\rho g} = \frac{V_2^2}{2g} - \frac{V_1^2}{2g}$$

$$h = \frac{V_2^2 - V_1^2}{2g}$$

$$2g h = V_2^2 - V_1^2$$

$$V_2 = \sqrt{2gh + V_1^2} \quad (5.8)$$

Now , section 2 is at the ( vena – contracta ) and  $A_2$  represents the area at the ( vena – contracta) . If the  $A_o$  is the area of orifice , then we have :

$$C_c = \frac{A_2}{A_o}$$

Where ,  $C_c$  - Coefficient of contraction .

$$\text{Then , } A_2 = C_c A_o$$

From continuity equation , we have ,  $A_1 V_1 = A_2 V_2$

$$V_1 = \frac{A_2}{A_1} V_2 = \frac{A_o C_c}{A_1} V_2$$

Substituting the value of  $V_1$  in equation ( 5.8 ) :

$$V_2 = \sqrt{2gh + \frac{A_o^2 C_c^2 V_2^2}{A_1^2}}$$

$$V_2 = \frac{\sqrt{2gh}}{\sqrt{1 - \left(\frac{A_0}{A_1}\right)^2 C_c^2}}, \text{ After simplified , } V_2 = \frac{A_1 \sqrt{2gh}}{C_c \sqrt{A_1^2 - A_0^2}}$$

$$\text{The discharge } Q = C_d V_2 A_2 = C_d V_2 A_0 C_c = \frac{C_d A_0 C_c A_1 \sqrt{2gh}}{C_c \sqrt{A_1^2 - A_0^2}}$$

$$Q = \frac{C_d A_0 A_1 \sqrt{2gh}}{\sqrt{A_1^2 - A_0^2}} \quad (5.9)$$

Where ,

$C_d$  - Coefficient of discharge for orifice meter .

### 3. Pitot – tube :

It is a device used for measuring the velocity of flow at any point in a pipe or a channel . It is based on the principle that if the velocity of flow at a point becomes zero, the pressure there is increased due to the conversion of the kinetic energy into pressure energy .

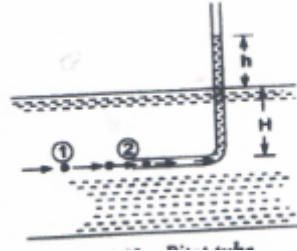


Fig.(5.4 )

Applying Bernoulli's between points 1 & 2 , we get :

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_2$$

$Z_1 = Z_2$  , because the points 1 & 2 are on the same line , and  $V_2 = 0$  .

$$\frac{P_1}{\rho g} + \frac{V_1^2}{2g} = \frac{P_2}{\rho g}$$

$$H + \frac{V_1^2}{2g} = (h + H)$$

$$\frac{V_1^2}{2g} = h \quad , \quad V_1 = \sqrt{2gh}$$

In this equation , the velocity  $V_1$  is theoretical velocity , but the actual velocity is :

$$(V_1)_{\text{actual}} = C_v \sqrt{2gh} \quad (5.10)$$

There are many arrangements with Pitot – tube ( as shown in Figures ) :

1 – Pitot- tube along with a vertical piezometer tube , as shown in Fig.(5.5 )

2 – Pitot –tube connected with piezometer tube as shown in Fig.( 5. 6 ).

3 – Pitot – tube and vertical piezometer tube connected with a differential U – tube manometer as shown in Fig.( 5. 7 ).

4 – Pitot – tube , which consists of two circular concentric tubes one inside , the other with some annular space in between as shown in Fig. ( 5.8 ). The outlet of these two tubes are connected to the differential manometer where the differential of pressure head ( h ) is measured by knowing the difference of the levels of the manometer liquid , say x , then :

$$h = x \left[ \frac{S_m}{S_o} - 1 \right]$$

