

Answer the following by choose the correct:

- Ideal fluid is one has \_\_\_\_d\_\_\_\_.  
(a) No viscosity (b) No surface tension (c) No compressibility (d) All of the above
- This shear stress is proportional to the rate of change of velocity with respect to y. It is denoted as  $\tau$  and mathematically \_\_\_\_a\_\_\_\_.  
(a)  $\tau = \mu \frac{du}{dy}$  (b)  $\tau = \frac{1}{\mu} \frac{du}{dy}$  (c)  $\tau = \frac{1}{\mu} \frac{dy}{du}$  (d)  $\tau = \mu \frac{dy}{du}$
- Reynolds number is defined as \_\_\_\_c\_\_\_\_ for a flow on flat plate.  
(a)  $Re_L = \frac{\rho u L^2}{\mu}$  (b)  $Re_L = \frac{u L^2}{\mu}$  (c)  $Re_L = \frac{\rho u L}{\mu}$  (d)  $Re_L = \frac{\rho u}{\mu}$
- For laminar flow over a flat plate, the Reynolds number becomes less than \_\_\_\_d\_\_\_\_  
(a)  $2 \times 10^4$  (b)  $7 \times 10^7$  (c)  $10 \times 10^5$  (d)  $5 \times 10^5$
- For turbulent flow in the pipe  $Re_d$  be greater than \_\_\_\_c\_\_\_\_  
(a) 1000 (b) 2000 (c) 2300 (d) 10000
- Prandtl number (Pr) is the ratio of kinematic viscosity to thermal diffusivity and mathematically denoted as \_\_\_\_d\_\_\_\_.  
(a)  $Pr = \frac{\mu C_p}{k}$  (b)  $Pr = \frac{\rho \nu C_p}{k}$  (c)  $Pr = \frac{\nu}{\alpha}$  (d) All of the above
- Nusselt Number for flow in tube is denoted mathematically as \_\_\_\_\_.  
(a)  $Nu_d = \frac{d.k}{h}$  (b)  $Nu_d = \frac{h.d}{k}$  (c)  $Nu_d = \frac{k}{h.d}$  (d)  $Nu_d = \frac{h}{k.d}$
- Air at atmospheric pressure and  $200^\circ\text{C}$  flows over a plate with velocity of 5m/s. The plate is 15mm wide and is maintained at a temperature of  $120^\circ\text{C}$ . Calculate the Reynold's Number at distance of 0.5 meter and the local and average heat transfer coefficient \_\_\_\_a\_\_\_\_. The properties at film-temperature are  $\rho=0.815\text{kg/m}^3$ ,  $\mu=24.5 \times 10^{-6}\text{N.s/m}^2$ ,  $Pr=0.7$ ,  $k=0.0364\text{W/m.K}$ .  
(a)  $0.831 \times 10^5, 6.188\text{W/m}^2.\text{K}, 12.376\text{W/m}^2.\text{K}$   
(b) 6.188,  $0.831 \times 10^5\text{W/m}^2.\text{K}, 12.376\text{W/m}^2.\text{K}$   
(c)  $0.831 \times 10^5, 12.376\text{W/m}^2.\text{K}, 6.188\text{W/m}^2.\text{K}$   
(d)  $0.831 \times 10^5, 74.256\text{W/m}^2.\text{K}, 12.376\text{W/m}^2.\text{K}$

9. The hydraulic diameter is defined as c.

(a)  $d_h = \frac{4P}{A}$     (b)  $d_h = \frac{A}{4P}$     (c)  $d_h = \frac{4A}{P}$     (d)  $d_h = \frac{2A}{P}$

10. For turbulent flow in tube the Nusselt Number is calculated by Following relation a.

(a)  $\overline{Nu} = 0.023 (Re_d)^{0.8} (Pr)^{1/3}$

(b)  $\overline{Nu} = 0.023 (Re_L)^{0.8} (Pr)^{1/3}$

(c)  $\overline{Nu} = 0.023 (Re_d)^{0.4} (Pr)^{1/3}$

(d)  $\overline{Nu} = 0.023 (Re_d)^{0.8} (Pe)^{1/2}$

11. The convective heat transfer coefficient in laminar flow over a flat plate c

(a) increases if a lighter fluid is used

(b) increases if a higher viscosity fluid is used

(c) increases if higher velocities are used

(d) increases with distance.

12. Reynolds number for flow in pipe is c

(a)  $Re = \frac{Ldu}{\mu}$

(b)  $Re = \frac{\rho u d}{\nu}$

(c)  $Re = \frac{\rho d u}{\mu}$

(d)  $Re = \frac{d.u}{\mu}$

13. The friction factor in the laminar region is proportional to d

(a)  $Re^{0.5}$     (b)  $Re^{0.2}$     (c)  $Re^{-0.2}$     (d)  $Re^{-0.5}$

14. In pipe flow, the average convection coefficient

(a) will be higher in rough pipes

(b) will be higher in smooth pipes

(c) Roughness affects only pressure drop and not the convection coefficient

(d) Only Reynolds and Prandtl numbers influence the convection coefficient and not the roughness.

15. Air at 20°C flows over a 4-m-long and 3-m-wide surface of a plate whose temperature is 80°C with a velocity of 5 m/s. The rate of heat transfer from the laminar flow region of the surface is \_\_\_c\_\_\_. (For air, use  $k = 0.02735 \text{ W/m.K}$ ,  $Pr = 0.7228$ ,  $\nu = 1.798 \times 10^{-5} \text{ m}^2/\text{s}$ )

- (a) 950 W    (b) 1037 W    (c) 2074 W    (d) 2640 W

16. The normal automobile radiator is a heat exchanger of the type \_\_\_d\_\_\_.

- (a) Direct contact  
(b) Parallel flow  
(c) Counter flow  
(d) Cross flow

17. The requirement of transfer of a large heat is usually met by \_\_\_d\_\_\_.

- (a) Increase the length of the tube  
(b) Decreasing the diameter of the tube  
(c) Increase the number of tubes  
(d) Having multiple tube of shell passes

18. In a heat exchanger with one fluid evaporating or condensing, the surface area required is least in \_\_\_b\_\_\_.

- (a) Parallel flow  
(b) Counter flow  
(c) Cross flow  
(d) Same in parallel, counter and cross flow arrangements

19. In a counter-flow heat exchanger, cold fluid enters at 30°C and leaves at 50°C, whereas the hot fluid enters at 150°C and leaves at 130°C. The mean temperature difference for this case is \_\_\_c\_\_\_.

- (a) 20°C  
(b) 80°C  
(c) 100°C

(d) Indeterminate

20. In a heat exchanger, the hot liquid enters with a temperature of  $180^{\circ}\text{C}$  and leaves at  $160^{\circ}\text{C}$ . The cooling fluid enters at  $30^{\circ}\text{C}$  and leaves at  $110^{\circ}\text{C}$ . The capacity ratio of the heat exchanger is \_\_\_a\_\_\_.

(a) 0.25

(b) 1.5

(c) 0.33

(d) 0.2

21. The overall heat transfer coefficient for a shell and tube heat exchanger for clean surfaces is  $U_o=400\text{W/m}^2.\text{K}$ . The fouling after one year of operation is found to be  $h_o=2000\text{W/m}^2.\text{K}$ . The overall heat transfer coefficient at this time is \_\_\_c\_\_\_.

(a)  $1200\text{W/m}^2.\text{K}$  (b)  $894\text{W/m}^2.\text{K}$  (c)  $333\text{W/m}^2.\text{K}$  (d)  $287\text{W/m}^2.\text{K}$

22. A correction of LMTD is necessary in case of \_\_\_a\_\_\_ heat exchanger.

(a) Cross flow

(b) Parallel flow

(c) Counter current

(d) All of theses

23. Fouling factor is used \_\_\_d\_\_\_

(a) In heat exchanger design as a safety factor

(b) In case of Newtonian fluids

(c) When a liquid exchanges heat with a gas

(d) None of theses

24. In a shell and tube heat exchanger, baffles are provided on the shell side to \_\_\_d\_\_\_.

(a) Improve heat transfer.

(b) Provide support for tubes

(c) Prevent stagnation of shell side fluid

(d) All of these

25. In a two-fluid heat exchanger, the inlet and outlet temperature of the hot fluid are  $65^{\circ}\text{C}$  and  $40^{\circ}\text{C}$  respectively. For the cold fluid these are  $15^{\circ}\text{C}$  and  $42^{\circ}\text{C}$ . The heat exchanger is a \_\_\_\_ b \_\_\_\_.

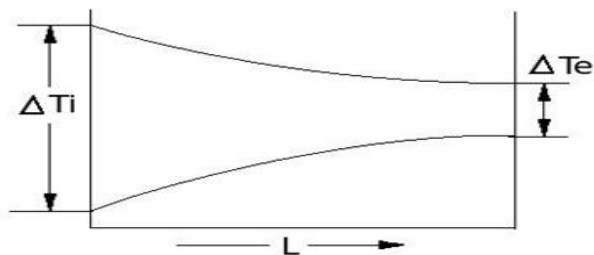
- (a) Cross-flow heat exchanger
- (b) Counter-flow heat exchanger
- (c) Parallel-flow heat exchanger
- (d) None of these

26. In case of heat exchanger, the value of LMTD should be \_\_\_\_ b \_\_\_\_.

- (a) As small as possible
- (b) As large as possible
- (c) Constant
- (d) Has a specific level of temperature which depends on the size of the heat exchanger

27. Which type of flow in heat exchanger is represented in below diagram?

\_\_\_\_ a \_\_\_\_.



*Temperature Profile of Fluids in Heat Exchanger*

- (a) Parallel flow heat exchanger
- (b) Counter flow heat exchanger
- (c) Cross flow heat exchanger
- (d) None of the above

28. For the same inlet and exit temperatures of two fluids, the LMTD for counter flow is always \_\_\_\_ b \_\_\_\_.

- (a) Smaller than LMTD for parallel flow
- (b) Greater than LMTD for parallel flow
- (c) Same as LMTD for parallel flow

(d) Unpredictable

29. For the same heat transfer  $Q$  and same overall heat transfer coefficient  $U_o$ , surface area required for parallel flow heat operation is always \_\_\_\_b\_\_\_\_.

(a) Less than that for counter flow

(b) More than that for counter flow

(c) Same as that for counter flow

(d) Unpredictable

30. For the same heat transfer  $Q$  and same overall heat transfer coefficient  $U_o$ , surface area required for cross flow operation is always \_\_\_\_a\_\_\_\_.

(a) Less than LMTD for parallel flow

(b) More than LMTD for parallel flow

(c) Same as LMTD for parallel flow

(d) Unpredictable

31. In a direct contact heat exchanger, there is \_\_\_\_c\_\_\_\_

(a) Mass transfer

(b) Heat transfer

(c) Heat & mass transfer

(d) None

32. In a condenser, the temperature of the hot fluid is \_\_c\_\_.

(a) Decreasing

(b) Increasing

(c) Remains constant (d) None

33. The sequence of the modes of heat transfer in case of a heat exchanger are \_\_\_\_c\_\_\_\_.

(a) Cond. + conv. + rad.

(b) Conv. + rad. + conv.

(c) Conv. + cond. + conv.

(d) None

34. a correction factor 'F' to calculate the rate of heat transfer in case of a \_\_\_\_c\_\_\_\_.

(a) Parallel flow heat exchanger

(b) Counter flow heat exchanger

(c) Cross flow heat exchanger

(d) None

35. The equation of LMTD is \_\_\_\_c\_\_\_\_.

(a)  $(\Delta T_a + \Delta T_b) / \ln(\Delta T_a / \Delta T_b)$

(b)  $(\Delta T_a \Delta T_b) / \ln(\Delta T_a / \Delta T_b)$

(c)  $(\Delta T_a - \Delta T_b) / \ln(\Delta T_a / \Delta T_b)$

(d) *None*

36. The general equation for heat transfer rate  $\dot{Q}$ , is expressed as: \_\_\_\_c\_\_\_\_

(a)  $A\Delta T/U$  (b)  $U/A\Delta T$  (c)  $AU\Delta T$  (d)  $UA/\Delta T$